# Feasibility Study of Time-Intensity-Based Blood Flow Measurements Using Deconvolution

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Ul tra sonic con trast agents have been used to en hance the acous tic back scat tered in ten sity of blood and to as sist the as sess ment of blood flow pa ram e ters. One ex am ple is the time-intensity method based on the in di ca tor-dilution the ory. In this case, a mix ing cham ber model can be em ployed to de scribe the concentration of the contrast agent as a function of time. By measuring the time in tensities at both the input and output of the blood mixing chamber, blood flow information can be obtained if proper deconvolution tech niques are ap plied. Note that most deconvolution tech niques as sume a lin ear and time in vari ant (LTI) system for the mixing of the contrast agent with blood. In this paper, the hypothesis that a blood mix ing cham ber is an LTI sys tem was tested. Several as pects were studied. One as pect was the lin ear relation ship be tween the concentration of the contrast agent and the back scattered in tensity. The other as pect was the dependence of the derived time constants on the concentration. The concept of an ef fec tive mix ing vol ume was also in tro duced and eval u ated. Finally, the in put and the out put time con stants were mea sured and com pared to the ory under the LTI as sumption. Extensive experiments were per formed. Two invitro flow models were constructed and two con trast agents were used. Re sults in dicated that the LTI as sumption does not hold and quantitative flow estimation is generally not possible. None the less, the in dica tor-dilution the ory can still be ap plied if only rel a tive measure ments of the flow rate are required.

KEY WORDS: Blood flow es ti mation; deconvolution; effec tive mix ing volume; time-intensity curve; ultra sonic con trast agent.

# 1. INTRODUCTION

Ultrasonic contrast agents are used to enhance the acoustic backscattered intensity of blood. They improve blood flow detection and of fer possibilities to visualize per fusion conditions. Several recent studies have focused on *in vivo* and *in vitro* flow measure ments based on the indicator-dilution theory.<sup>16</sup> The indicator-dilution theory provides a mathematical model for estimating hemodynamic parameters using changes in the back scattered in tensity as a function of time (i.e., the time-intensity curve).<sup>711</sup> It has been shown that rel a tive change in the wash-out rate of the time-intensity curve is linearly proportional to the volu metric flow rate.<sup>5</sup> It has also been shown that the peak intensity of the time-intensity curve is approximately linearly proportional to the volume concentration of the injection contrast agent.<sup>12</sup> Thus, the possibility for quantitative per fusion anal y sis using the time-intensity curve has been demonstrated.

The concentration of the contrast agent as a function of time can be math e mat i cally derived by modeling the flow system as a series of blood mixing chambers. Each mixing chamber is described by a transfer function relating the indicator concentration entering (i.e., in put) and leaving (i.e., out put) the chamber as a function of time. With a bolus in jection, a good correlation be tween time constants derived from the time-intensity curve and the volumetric flow rate can generally be found, if the acoustic intensity is linearly proportional to the concentration.<sup>4</sup> How ever, the time-intensity based methods are not as effective when the injec tion site is far away from the mea sure ment site. <sup>12</sup> The sit u a tion can be viewed as the case where there are more than one mix ing cham ber be tween the in jec tion site and mea sure ment site. Thus, the in put func tion of the last mix ing cham ber has a pro longed du ra tion. When a pro longed in jec tion is in tro duced, the out put time-intensity curve re flects not only the dilution pro cess in the mix ing cham ber, the in put must also be taken into ac count.

To take into account the input function, the output time-intensity curve of the mixing cham ber can be represented as the convolution of the input function and transfer function of the mixing chamber.<sup>13-16</sup> Assuming a linear and time-invariant (LTI) system, the transfer function of the mix ing cham ber can be obtained by deconvolution tech niques if both the input and the output time-intensity curves are available. However, most deconvolution algorithms proposed to date were applied to an alyze simulation data. Efficacy of the deconvolution algorithms on *in vitro* and *in vivo* data is not yet evaluated.

A fundamental hypothesis that needs to be tested be fore in vestigating the deconvolution techniques is the as sumption that the blood mixing chamber is LTI. <sup>*n*</sup> In other words, it is necessary to verify if the acoustic back scattered intensity is linearly proportional to the concentration such that the measured time-intensity curve reasonably represents the temporal change of the concentration of the contrast agent. In fluence of the concentration on flow estimation has been preciously discussed. <sup>2-3, 11-12</sup> The linear relation ship be tween the concentration and parameters such as the area under the time-intensity curve and the peak intensity was found if the concentration was within a certain range. One primary pur pose of this study is to invest igate not only the relation ship be tween the acoustic in tensity and the concentration, but also effects of the concentration on flow estimation results. In addition, bot h a compartment flow model and per fusion flow model will be used.

Another fac tor af fect ing the LTI as sump tion is the effect of the cham ber size on blood mix ing. In other words, the effect ive vol ume may be different from the physical vol ume of the mixing chamber. <sup>18</sup> If the contrast agent does not mix completely with liquid within the mixing chamber, the effective dilution vol ume is smaller than the physical vol ume of the mixing chamber. Be cause the wash-out rate of the contrast agent depends on both the vol ume tric flow rate and the vol ume of the mixing chamber, quant it a tive flow est imation is not possible with out the knowl edge of the effective mixing vol ume. In other words, the indicator-dilution the ory can only be used to est imate the effective vol ume, in stead of the physical volume. In fluence of the effective vol ume on the time-intensity based flow est imation is also studied in this paper.

Finally, an other pur pose of this study is to in ves ti gate the valid ity of the LTI as sumption by comparing the input time constant to the out put time constant. The relation ship between the input time constant and the out put time constant are mathematically derived and compared to the measurement results. The experiments in this study were performed with both a compart ment model and a perfusion model.<sup>99</sup> Each model had two configurations for bolus injections and prolonged injections, respectively. Experimental results are summarized with a discussion on the applicability and limitations of the time-intensity based flow estimation techniques.

### 2. MATERIALS AND METHODS

#### A. Basicprinciples

When a cer tain amount of in di ca tor so lu tion is in put into the flow sys tem, the con cen tration at the sys tem out put can be de scribed based on the in di ca tor-dilution the ory. How ever, the con cen tra tion of the ul tra sonic con trast agent is not di rectly mea sured in prac tice. In-



FIG. 1. Il lus tration of the in put and the out put of a mix ing cham ber.

stead, the back scat tered acoust ic in tensity is used to represent the concentration of the contrast agent. The following discussion on the mixing chamber model assumes that the back scattered intensity is a linear function of the concentration of the contrast agent. The valid ity of this as sumption will be studied in the next section.

A di a gram of the mix ing cham ber is de picted in fig ure 1. The echo in ten sity mea sured at the out put of a mix ing cham ber, de noted by  $I_o(t)$ , de pends on the in put function  $I_i(t)$  and the transferfunction h(t). If the system is LTI, the out put function can be expressed as the con volution of the in put function and transfer function of the mix ing cham ber. <sup>1</sup> In other words,

$$I_O(t) = I_I(t) \otimes h(t), \tag{1}$$

where  $\otimes$  stands for convolution and h(t) is the trans fer function of the mix ing cham ber. The transfer function h(t) contains char acter is tics of the mix ing cham ber and is given by

$$h(t) = \begin{cases} 0 & t < 0 \\ \frac{1}{\tau} e^{-t/\tau} & t > 0 \end{cases}$$
(2)

where  $\tau$  is con sid ered as the sys tem's tran sit time (i.e., in verse of the wash-out rate) and is proportional to the mixing chamber volume and inversely proportional to the volumetric flow rate.<sup>1</sup> Equation (1) in di cates that deconvolution tech niques can be ap plied to es ti mate the transfer function of a mixing chamber if both the input and the output time-intensity curves are available. After the transfer function is determined, blood flow parameters, such as the wash-out rate, can then be ob tained.

The time-intensity curve is used to de rive two pa ram e ters in this study. One is the mean transit time (MTT) and the other is the area un der curve (AUC). The MTT is de fined as

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$$MTT = \frac{\int_0^\infty tx(t)dt}{\int_0^\infty x(t)dt},$$
(3)

where x(t) is either the mea sured time-intensity curve or the derived trans fer function of the mix ing cham ber. The MTT represents the time for the entire fluid volume to pass though the mix ing cham ber. Ac cording to the in dicator-dilution the ory, there is an inverse relation between the flow rate and the MTT. If the trans fer function is defined in Eq. (2), it can be shown that

$$MTT = \tau = \frac{V}{Q},\tag{4}$$

where V is the volume of mixing cham ber and Q is the volumetric flow rate. In this study, the flow rate ranged from 500 to 1100 ml/min and the size of the mixing cham bers ranged from 200 to 930 ml.

Based on Eqs. (1) and (2), it can also be shown that the MTT of the out put function  $(MTT_{out})$  equals the sum of the MTT of the in put function  $(MTT_n)$  and the MTT of the trans fer function of mix ing cham ber  $(MTT_{mix})$ .<sup>15</sup> In other words,

$$MTT_{aut} = MTT_{in} + MTT_{mix}.$$
(5)

To ver ify the LTI as sumption, the MTT derived from Eq. (5) will be compared with the value derived from Eq. (4).

Finally, the AUC defined as the following equation is used to test the linear relation ship between the concentration and back scattered in tensity.<sup>2</sup>

$$AUC = \int_{0}^{\infty} I_{o}(t)dt$$
<sup>(6)</sup>

#### **B.** Experimental setup

Two *in vitro* flow models were con structed. One was made of a spher i cal com part ment phan tom and the other was made of a per fu sion phan tom. <sup>9</sup> Fur ther more, each flow model had two different configurations. One was for bolus injection and the other was for prolonged in jec tions. Fig ure 2 shows a sin gle com part ment phan tom and fig ure 3 shows two com part ment phan toms in cas cade. If the in put has a short du ra tion com pared to the MTT of the mix ing cham ber, the out put in ten sity curve mea sured from the phan tom shown in fig ure 2 ap prox i mates the trans fer func tion of the mix ing cham ber (i.e., the in put is ap prox i mated as an im pulse). For the flow model shown in fig ure 3, on the other hand, the in put of cham ber A is also the out put of cham ber B. Thus, the time-intensity curve mea sured at the out put of cham ber A can be used to eval u ate the time-intensity based method when the in put has a prolonged duration.

The com part ment phan tom was made of an acrylic hol low sphere. Two sil i con tubes connecting to the sphere were fixed in par al lel with op po site flow di rec tions and im mersed in a LI ET AL



FIG. 2. Experimental setup for the compart ment phan tom.



FIG. 3. Experimental setup for two compart ment phan toms in cas cade.



FIG. 4. Experimental setup for the perfusion phantom.

wa ter tank. The di am e ter of the tubes was 8 mm. A 7-MHz lin ear ar ray trans ducer (L7-4, Ad vanced Tech nol ogy Lab or a tories, Bothell, WA, U.S.A.) was placed 2 cm above the tubes. The damper was used to sta bi lize the flow. To prevent recirculation of the con trast agent back into the phan tom, the wa ter in this sys tem only passed through the model once. In figure 2, the con trast agent was in jected to the tube at the front side of the sphere by a sy ringe. In fig ure 3, the in jec tion po si tion was at the in put side of cham ber B. The in put time-intensity curve of cham ber A was the trans fer function of cham ber B if the duration of the in put in jection was sufficiently short.

The other flow model was based on a perfusion phan tom made of a di al y sis cartridge. <sup>9</sup> Again, an ad di tional sphere was in serted be tween the in jec tion site and the perfusion phantom as the configuration for prolonged in jec tions. Sche matic di agrams of the two configurations are shown in fig ures 4 and 5, re spec tively. The di al y sis tube (C-12, TERUMO Co., To kyo, Japan) consisted of 8600 cap il lar ies with a di am e ter of 200  $\mu$ m and a length of 235 mm for each cap il lary, mak ing a to tal vol ume of 79 ml.

# C. Imageprocessing

The input and the output time-intensity curves were simultaneously measured using a commercial ultrasound machine (Ultramark 9, Advanced Technology Laboratories Inc., Bothell, WA, U.S.A.). The me chan i cal in dex (MI) was 0.7 with the im ag ing frame rate ranging from 20 to 30 Hz. The de struction of microbubbles due to the acoust ic power level was neg li gi ble based on the fact that the ratio of the in put AUC to the out put AUC was close to unity in all cases. Effects of postprocessing on the time in tensi ties were also ig nored be cause the im ages were ac quired prior to the postprocessing functions were ap plied. In addition, shadowing and other unwanted effects potentially resulting from the un even microbubble



FIG. 5. Experimental setup for the perfusion phantom in cascade with a compart ment phantom.

dis tri bu tion were not ob served in the gray-scale im ages. Gray-scale im ages of the trans verse view of the in put and the out put tubes were ac quired one frame per sec ond. A to tal of 300 image frames (i.e., 5 min utes) were ac quired and dig i tized by a frame grab ber (UPG401B, UP-MOST Corp., Tai pei, R.O.C.) and stored for off-line anal y sis. The im age size was 153 by 232 pix els cov er ing a 36 mm by 55 mm area. A typ i cal im age is shown in fig ure 6. The two re gions of in ter est de noted by the two cir cles cor re spond to the in put and the out put tubes. The im age data were con verted from the log a rith mic scale to the lin ear scale be fore the mean back scat tered in ten si ties in side the ROI were cal cu lated.

To ob tain a time-intensity curve, a cir cle was used to cover the in ner por tion of the tube. The in ten sities of the pix els in side the ROI were summed and the re sult was used as the in tensity at that par tic u lar time. The pro ce dures con tin ued un til all the 300 dig i tized gray-scale im ages were pro cessed.

To reduce noise in the time-intensity mea sure ments, the time-intensity curve is fit ted to a gamma function g(t) defined as the following

$$g(t) = \alpha (t - t_o)^{\gamma} e^{-\beta (t - t_o)}, \tag{7}$$

where  $t_0$  in dicates a delay time,  $\alpha$  and  $\beta$  are scaling fac tors and  $\gamma$  represents the skew ness. All flo-related parameters were calculated after gamma function fitting. Typical input and output time-intensity curves are shown in fig ure 7. Note that the dot ted lines cor re spond to the orig i nal mea sure ments and the solid lines are with curve fitting.

# **D.** Contrast agents

A commercial contrast agent (Levovist, <sup>®</sup> Schering, Berlin, Germany) and a self-made contrast agent were used. The self-made agent was made from hu man al bu min using the agi-

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FIG. 6. A typ i cal gray-scale im age show ing in ten si ties from both the in put and the out put tubes.



FIG.7. Typ i cal in put and out put time-intensity curves with (solid) and with out (dot ted) gamma fit ti ng.



**FIG. 8.** (a) AUC of the in put time-intensity curve and (b) MTT of the out put time-intensity curve vs. Levovist <sup>®</sup> concentration for the compart ment phan tom.

tationtechnique.<sup>4,20</sup> The size of the self-made microbubbles was es ti mated us ing a light micro scope (EMZ-TR, MEIJI Tech. Co., To kyo, Ja pan). The di am e ter of the self-made agent was about 20 to 50 mm.<sup>4</sup> The concentration of the al bu min-based contrast agent is pri marily de ter mined by the amount of air used when making the agent.

# 3. EXPERIMENTAL RESULTS

#### A. Concentration vs. mean transit time

Experiments were conducted to evaluate influence of the concentration of the contrast agent on the MTT es ti mates. A flow rate of 900 ml/min was used. For each case, the av er age and the stan dard de vi a tion were taken from three in de pend ent mea sure ments. The ex per imen tal setup is shown in fig ure 2, with the vol ume of the com part ment at 200 ml.

Figure 8(a) demonstrates the relationship between the AUC and the concentration of Levovist. <sup>®</sup> The av er age values are shown with the er ror bars represent ing +/- one stan dard deviation. Levovist <sup>®</sup> with four differ ent doses (0.5 g, 1.0 g, 1.5 g and 2.0 g) were mixed with 4 ml wa ter. It is shown that the AUC in creased with the Levovist <sup>®</sup> dose. Figure 8(b) shows the MTT es timated at four concentration levels (i.e., four differ ent doses). Theoretical values de rived from Eq. (4) were shown as the dashed line. Re sults in di cate that al though the AUC increased with the Levovist <sup>®</sup> concentration, the MTT estimates still varied with the concentration. The same experiments were also performed with the perfusion phantom shown in figure 4 un der the same experiment at conditions. Re sults are shown in figure 9.



FIG.9. (a) AUC of the in put time-intensity curve and (b) MTT of the out put time-intensity curve vs. Levovist <sup>®</sup> concentration for the perfusion phantom.

Again, the AUC in creased with the Levovist <sup>®</sup> concentration, but the MTT estimates were all smaller than the theoret i cal value (dashed line). Note that the theoret i cal value was calculated based on the sum of the volume of the car tridge (79 ml) and the volume of the connecting tubes (160 ml). If only the volume of the cartridge was considered, the dashed line becomes much closer to the measurement results.

Note that the MTT's for the per fu sion phan tom (fig ure 9(b)) ap pear to be much flat ter than those for the com part ment phan tom (fig ure 8(b)). One possible reason is the difference in the mix ing cam ber vol ume. In the per fu sion phan tom, the real di lu tion vol ume equaled the volume of the car tridge. The di lu tion vol ume of the com part ment phan tom, on the other hand, was larger than that of the per fu sion phan tom. In other words, the phys i cal vol ume may be larger than the effective volume.

The ex per i ments were also re peated us ing the al bu min-based con trast agent. Four ml of wa ter and 0.2 ml of 20% hu man al bu min were used in all cases. The different concentration levels cor re sponded to 0.2, 0.4, 0.6 and 0.8 ml of air, re spec tively. Fig ures 10 and 11 show the re sults from the com part ment phan tom and perfusion phan tom, re spec tively. In fig ures 10(a) and 11(a), the AUC in creases with the amount of air. The amount of air pri mar ily determines the concentration of the contrast agent. Figures 10(b) and 11(c) illustrate the MTT's estimated at different concentrations levels. Again, the MTT in creased with the concentration for the compartment phantom and stayed relatively constant for the perfusion phantom.

Re sults shown in fig ures 8-11 in di cate that the MTT gen er ally de pends on the con cen tration, al though the measure ments agree well with the the ory in certain sit u ations. In addition, the MTT estimates from the self-made agent have larger standard de viations than those from the commercial agent Levovist. <sup>®</sup> One possible reason is the size uniformity of microbubbles.



FIG. 10 (a) AUC of the in put time-intensity curve and (b) MTT of the out put time-intensity curve vs. concentration of the al bu min-based con trast agent for the com part ment phan tom.



**FIG.11.** (a) AUC of the in put time-intensity curve and (b) MTT of the out put time-intensity curve vs. concentration of the al bu min-based con trast agent for the per fu sion phan tom.



**FIG. 12.** MTT mea sured with the mix ing cham ber vol ume at (a) 200 ml, (b) 260 ml, (c) 580 ml, and (d) 930 ml. The air used for mak ing the con trast agent was 0.2 ml for all solid lines. In (a), 0.4 ml of air was used for the dashed lines, 0.6 ml for the dot-dashed line and 0.8 ml for the dot ted line.

For Levovist, <sup> $\circ$ </sup> 99% of the microbubbles are smaller 4  $\mu$ m whereas the size of the self-made agent ranged from 20 to 50  $\mu$ m. The size uni for mity may potentially affect the back scattered signalintensities.

#### B. Effective mixing volume

The MTT's were es ti mated from the out put time-intensity curves us ing the com part ment phan toms with different sizes and flow rates. The experimental setup is shown in figure 2 and the al bu min-based con trast agent was used. Re sults are shown in figure 12. In figure 12(a), the MTT's obtained at different concentration levels were shown. Again, the four concentration levels corresponded to 0.2, 0.4, 0.6 and 0.8 ml of air, respectively. Four ml of water, 0.2 ml of 20% hu man al bu min were used in all cases. The vol ume of the com part ment phan tom was 200 ml. Flow rates were 500, 700, 900 and 1100 ml/min. For each flow rate, five in depend ent mea sure ments were per formed. The hor i zon tal axis rep re sents the the oret i cal values ob tained from Eq. (4) and the verti cal axis shows the mea sured MTT. Mean values are shown as crosses with the er ror bars cor re sponding to +/- one stan dard de viation. Lin ear regres sion was per formed and the best-fit lines at different concentration levels are shown as the solid line (0.2 ml of air), the dashed line (0.4 ml of air), the dot-dashed line (0.6 ml of air)and the dot ted line (0.8 ml of air). The four cor re lation co ef fi cients be tween the MTT estimates and lin ear re gres sion lines were 0.94, 0.92, 0.94 and 0.93, re spec tively. In all cases, the estimated MTT is approximately inversely proportional to the volume flow rate Q, demon strating that the indicator-dilution the ory can be applied for relative volumetric flow measurements. However, absolute measurements are not possible due to the different MTT estimated at different concentration levels.

_	Flow rate	0.5 (l/min)	0.7(l/min)	<b>0.9</b> (l/min)	1.2 (l/min)
(a)	MTT(average)	23.85	16.00	13.20	11.97
	V/Q	24.00	17.14	13.33	10.91
	κ	0.99	0.93	0.99	1.10
(b)	MTT(average)	25.48	20.39	17.31	13.72
	V/Q	31.20	22.29	17.33	14.18
	κ	0.82	0.91	1.00	0.97
(c)	MTT(average)	41.24	35.30	26.69	24.03
	V/Q	69.60	49.71	38.67	31.64
	κ	0.59	0.71	0.69	0.76
(d)	MTT(average)	61.11	40.86	37.26	33.18
	<i>V/Q</i>	111.60	79.71	62.00	50.73

**TABLE1.** Sum mary of the estimated MTT's for four different volumes and four different flow rates. The volumes were (a) 200 ml, (b) 260 ml, (c) 580 ml, and (d) 930 ml.

Re sults shown in fig ures 12 (b) to 12 (d) cor re spond to the est i mated MTT's at differ ent flow rates and differ ent vol umes of the com part ment. As in fig ure 12(a), the flow rates were 500, 700, 900 and 1100 ml/min. The com part ment vol ume was 260 ml for fig ure 12(b), 580 ml for fig ure 12(c), and 930 ml for fig ure 12(d). The con centration of the con trast agent was fixed at 4 ml of water, 0.2 ml of 20% hu man al bu min and 0.2 ml of air. The three cor re lation co ef fi cients be tween the est i mated MTT's and the best-fit lines were 0.94, 0.92 and 0.88, respectively. The slopes of lin ear re gres sion the best-fit lines for fig ures 12(b) to 12(d) were 0.66, 0.48 and 0.45, respectively. The high correlation coefficients showed that relative flow est i mation is pos si ble with the time-intensity based meth ods. More over, it is shown that the slope de creased as the cham ber vol ume in creased. In other words, the effect twe mix ing volume changed with the physical volume. As the physical volume in creased, the ratio of the effect tive volume to the physical volume de creased.

The re sults at the 0.2 ml of air concentration level are sum marized in table 1. Tables 1(a) to 1(d) in clude re sults cor re sponding to the compart ment vol ume of 200, 260, 580 and 930 ml, re spec tively. In each case, the av er age es ti mated MTT's are shown in the sec ond row. The the oretical values based on Eq. (4) and the ratios ( $\kappa$ 's) of the estimated values to the the oretical values are shown in the third row and fourth row, re spec tively. If  $\kappa$  is close to one, it in dicates that the contrast agent mixes with the fluid completely within the chamber and the indicator-dilution the ory can be applied for absolute analy sis. Otherwise, only relat ive measures can be ob tained. As shown in table 1,  $\kappa$  is the close st to the one with the small est volume. It decreases as the compart ment volume in creases.

# C. Prolongedinjections

The experimental set ups shown in figures 3 and 5 were used to investigate effects of prolonged injection. For the setup shown in figure 3, the sizes of chambers A and B were 260 ml



FIG. 13. In put and out put MTT's mea sured with two compartment phan toms in cas cade (setup shown in fi gure 3).

and 200 ml, re spec tively. Four flow rates at 500, 700, 900 and 1100 ml/min were used. At each flow rate, five in de pend ent mea sure ments were per formed to ob tain mean and stan dard de vi a tion. The self-made con trast agent com posed of 0.2 ml of air, 4 ml of wa ter and 0.2 ml of 20% hu man al bu min was used.

Re sults are shown in fig ure 13. The hor i zon tal axis rep re sents the the oret i cal values obtained from Eq. (4) (i.e., 260 ml for cham ber A di vided by the flow rate) and the ver ti cal axis cor re sponds to var i ous MTT values. The dot ted line and the dashed line are the best-fit lines for the in put and out put MTT's of cham ber A based on the mea sured time-intensity curves. Ac cording to Eq. (5), the MTT for cham ber A can be ob tained by sub tracting the in put MTT from the out put MTT. The re sults are shown as the dot-dashed line. The mix ing cham ber MTT can also be found ac cord ing to Eq. (4) and re sults are shown as the solid line. Note that the solid line is sim ply a straight line with a slope of one. Ap par ently, the solid line is distinctly dif fer ent from the dot-dashed line in di cat ing that the concentration relation ship described by Eq. (1) may not be valid.

The same experiments were performed with the setup shown in figure 5. The size of chamber B was 200 ml and the chamber A was replaced with a di al y sis car tridge. Re sults are shown in figure 14. Sim i lar to the re sults shown in figure 13, the con volution relation ship be tween the in put time-intensity curve and the out put time-intensity curve again does not hold. None the less, all the mea sure ment re sults shown in figures 13 and 14 in dicate that the MTT is approximately inversely proportional to the volume flow rate Q.

## 4. CONCLUSION

The hy poth e sis that mix ing of the con trast agent is an LTI process was tested in this paper. Such a study is critical in determining if deconvolution techniques can be applied for quantiLI ET AL



**FIG. 14.** In put and out put MTT's measured with the per fu sion phan tom in cas cade with a compart ment phantom (setup shown in fig ure 5).

ta tive blood flow est i mation. Re sults in di cated that al though the back scattered in ten sity increased with the concentration of the contrast agent, the mea sured MTT's also varied as the concentration varied. In addition, the MTT's of the mixing chamber derived based on Eq. (5) were different from the MTT's obtained based on Eq. (4). There fore, it is concluded that the mixing process is generally not LTI and deconvolution techniques cannot be applied for measuring the ab solute flow rate. More over, ta ble I showed that the MTT estimates were affected by both the volume of the mixing chamber and the flow rate. In general, the MTT estimates were close st to the the ory with a smaller mixing chamber and at a higher flow rate. Al though deconvolution techniques are generally not applicable, results in figures 12 to 14 showed that a linear relationship was still present be tween the measured MTT values and the oretical MTT values. Thus, time-intensity based methods are still feasible if only relative flow analysis is required.

In an other study of this re search project, the com part ment flow phan tom was placed both vertically and horizontally. Re sults showed that both configurations produced good relative es ti mates of flow parameters. Hence, in fluence of microbubbles buoy ancy can be ig nored when the larger di ameter self-made agent was used.

Only con stant flows were con sid ered in this paper. In practice, pulsatile flows are present and the trans fer function be comes time-varying since the time constant is also a function of the flow rate. Effects of the pulsatile flows on flow est i mation need to be fur ther studied. New methods based on both the in put and the out put time-intensity curves are also of great in terest.

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